



**AUSTRALIAN ATOMIC ENERGY COMMISSION
RESEARCH ESTABLISHMENT
LUCAS HEIGHTS**

**TWIST - A NUMERICAL TECHNIQUE FOR CALCULATING THE STEADY-STATE
MASS FRACTION VARIATION IN AN AXI-SYMMETRIC BINARY
GAS MIXTURE SUBJECTED TO PRESSURE GRADIENTS**

by

**N. SPINKS
D.J. WILSON**

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ABSTRACT

The equation for diffusion in a binary gas mixture is integrated over each of a number of elements into which the R-Z system volume is divided. The resulting equations are soluble using the TWIST programme to give the mass fraction variation through the system. The Programme is suitable for analysis of any device which utilises pressure diffusion for the separation of a binary gas mixture, the components of which have approximately equal molecular weights and is describable in the R-Z coordinate system. Applications include the centrifuge, the vortex tube and the Vortex Matrix.

A knowledge of the mixture mass flow and pressure distribution throughout the system is assumed. A weakness of this method is the requirement of a fine subdivision of the system volume when such flows are large.

The TWIST programme has been applied to a counter-current centrifuge and the results compared with those from Cohen's theory.

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FIGURE 1 A finite volume element with neighbours.

FIGURE 2 Counter-current flow distribution for TWIST.

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APPENDIX A - Cohen's Approach for the Counter-Current Centrifuge.

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APPENDIX C - Programme Listing.

1. INTRODUCTION

Although the time dependant behaviour of an isotope separating device can be quite an important subject, much can be learnt from a study of its steady-state behaviour.

Pressure diffusion is employed in most separative devices, including the ultra-centrifuge, the vortex tube, and the Becker Nozzle. We concentrate here on those devices in which the binary gas mixture is caused to rotate about an axis.

Cylindrical coordinates are convenient for the description of these systems, but to avoid the calculational complexity and expense of a full 3D solution, it is necessary to eliminate at least one of the three spatial variables, R , Z or θ . For the ultra-centrifuge and, to a lesser extent, the vortex tube, RZ modelling should be satisfactory. For the vortex matrix, an RZ model could be considered adequate.

Rotation of the gas induces a centrifugal field which, whilst it has no intrinsic separating effect, induces a pressure gradient which performs the separation. Although its tangential component is predominant, the gas velocity will also have radial and axial components. These 'secondary' flows will affect the radial pressure gradient and will also induce an axial pressure gradient. As it is the resultant pressure gradient vector which performs the separation, we must allow for both radial and axial components. This is particularly necessary for the vortex tube device where rapid axial deterioration of the radial pressure gradient could occur.

It is assumed that the pressure field and secondary flow distributions are known throughout the volume of the device. A knowledge of the secondary flows is required for the calculation of mass transport resulting from bulk fluid flow.

It is further assumed that the difference between the molecular weights of the component gases is small so that the mixture molecular weight can be taken to be independent of position.

For the complex secondary flow patterns possible in a vortex device, it appears that the mass diffusion equations can only be solved by numerical methods. For more simple secondary flows in certain devices, analytical solutions are available (Cohen 1951), and their use is recommended. Cohen obtained an analytical solution for the counter-current centrifuge by neglecting the effect of axial diffusion on the radial concentration gradient. Here the numerical method would be useful only to cross-check results.

Before proceeding to the numerical method, the mass diffusion equation is

cast in dimensionless form. The input data for the resulting computer programme (see Appendix B) becomes dimensionless, thus avoiding the restrictions of a specific set of units. In addition, the result of any computer run is easily recognisable as being applicable to any system described by the particular set of dimensionless data.

The numerical method seeks to evaluate the mass fraction at the centre of each of a number of elements into which the volume is divided. A feature of this method is the use of an integral rather than a differential approach; this conserves matter irrespective of the coarseness of subdivision of the system volume.

The method produces a set of simultaneous equations for the unknown mass fractions. Following a description of the computer programme TWIST for the solution of these equations, an application of the programme to a counter-current centrifuge is discussed, with the results compared to those from Cohen's theory.

2. DIMENSIONLESS EQUATIONS

For a binary mixture, the steady-state equation of continuity of species A is, from equation 18.3-4 of Bird, Stewart and Lightfoot (1960),

$$\nabla \cdot (\rho_A v + j_A) = 0 \quad \dots(1)$$

where v and j_A are vector quantities, v being the mass averaged velocity and j_A being the mass flux of species A with respect to v ; ρ_A is the density of species A.

Considering only ordinary (concentration) diffusion and pressure diffusion fluxes to be relevant, then

$$j_A = j_A^{(c)} + j_A^{(P)} \quad \dots(2)$$

From equation c of table 16.2-1 of Bird et al. (1960)

$$j_A^{(c)} = -\rho D \nabla \omega_A \quad \dots(3)$$

where ρ is the mixture density, D is the mass diffusivity and ω_A is the mass fraction of species A. From equation 18.4-9 of Bird et al. (1960)

$$j_A^{(P)} = \frac{-c^2}{\rho \cdot R \cdot T} \cdot M_A \cdot M_B \cdot D \left[x_A \cdot M_A \left(\frac{\bar{v}_A}{M_A} - \frac{1}{\rho} \right) \cdot \nabla P \right] \quad \dots(4)$$

where c is the molar density and x_A is the mole fraction of A, the lighter of the species, D is the diffusion coefficient, M the molecular weight, R the gas constant and P and T are the pressure and temperature. As it is preferable to

work in terms of mass fraction, we write

$$c \cdot x_A \cdot M_A = \rho \cdot \omega_A \quad \dots (5)$$

This gives,

$$j_A^{(P)} = \frac{c}{R \cdot T} \cdot M_B \cdot D \cdot \omega_A (\bar{V}_A - M_A/\rho) \cdot \nabla P \quad \dots (6)$$

For a perfect gas,

$$\bar{V}_A^{-1} = c = \frac{\rho}{M} = \rho \left(\frac{\omega_A}{M_A} + \frac{1-\omega_A}{M_B} \right) \quad \dots (7)$$

so,

$$j_A^{(P)} = - \rho D \cdot \frac{\Delta M}{M} \cdot \omega \cdot (1-\omega) \cdot \nabla \ln P \quad \dots (8)$$

Substituting $\rho_A = \rho \cdot \omega_A$ in equation 1, we can drop the subscript A and use equations 3 and 8 to obtain

$$\nabla \cdot (\rho v \omega) = \nabla \cdot \left(\rho D \nabla \omega + \rho D \cdot \frac{\Delta M}{M} \cdot \omega \cdot (1-\omega) \cdot \nabla \cdot \ln P \right) \quad \dots (9)$$

Defining a characteristic length L^* and a characteristic product of density and diffusion coefficient $(\rho D)^*$, and then multiplying equation 9 through by $(L^*)^2/(\rho D)^*$, the following dimensionless form is achieved:

$$\tilde{\nabla} \cdot \tilde{G} \omega = \tilde{\nabla} \cdot \left(\eta \cdot \tilde{\nabla} \omega + \eta \cdot \frac{D}{D} \cdot \frac{\Delta M}{M} \omega \cdot (1-\omega) \tilde{\nabla} \ln P \right) \quad \dots (10)$$

where $\tilde{\nabla} = L^* \nabla$

and \tilde{G} is the dimensionless mass flux

$$\tilde{G} = \frac{\rho v}{(\rho D)^*/L^*} \quad \dots (11)$$

Also,

$$\eta = \frac{\rho D}{(\rho D)^*} \quad \dots (12)$$

and, since it is generally accepted that ρD is independent of pressure, η reflects the temperature dependence of ρD .

Integrating equation 10 over a volume enclosed by a surface S, then by Green's theorem

$$-\int \tilde{G} \omega \tilde{d}S + \int \eta \tilde{\nabla} \omega \cdot \tilde{d}S + \int \eta \frac{D}{D} \frac{\Delta M}{M} \omega \cdot (1-\omega) \tilde{\nabla} \ln P \cdot \tilde{d}S = 0 \quad \dots (13)$$

where

$$\tilde{S} = S/(L^*)^2 \quad \dots(14)$$

The *tilda* in equation 13 can be discarded provided it is noted that all length measurements must be expressed as multiples of L^* and all mass fluxes as multiples of $(\rho D)^*/L^*$. It follows that any mass flow integrated over a given area must be expressed as a multiple of $(\rho D)^*/L^*$. With this understanding, we can write,

$$-\int G\omega \cdot dS + \int \eta \cdot \nabla\omega \, dS + \int \eta \cdot \frac{D}{D} \cdot \frac{\Delta M}{M} \cdot \omega(1-\omega) \nabla \ln P \cdot dS = 0 \quad \dots(15)$$

3. FINITE DIFFERENCE APPROXIMATION

3.1 Introduction

The volume of the cylindrical system is divided into a number of intervals separated by surfaces with areas

$$A_i^{(Z)} = \pi (r_{i+1}^2 - r_i^2) = \pi (r_{i+1} + r_i) \delta r_i \quad \dots(16)$$

$$\text{and } A_{i,j}^{(R)} = 2\pi r_i (z_{j+1} - z_j) = 2\pi r_i \delta z_j \quad \dots(17)$$

where r_i and z_j are the coordinates of mesh lines defining the intervals. Figure 1 shows how the mass flow rates $w_{ij}^{(Z)}$ and $w_{ij}^{(R)}$ are defined at the surfaces of each interval whilst other quantities ω_{ij} are defined at the mid points of each interval.

3.2 Convective Flow

In applying equation 15 to one of the above intervals, we first consider the term representing convective flow of the desired species across the surface. We require values of ω at the surfaces, and these are obtained by linear interpolation. For example, the value of ω corresponding to $w_{i,j}^{(Z)}$ is

$$\omega_{i,j-\frac{1}{2}} = (1-q_j^{(Z)}) \omega_{i,j} + q_j^{(Z)} \omega_{i,j-1} \quad \dots(18)$$

where

$$q_j^{(Z)} = \delta z_j / (\delta z_j + \delta z_{j-1}) \quad \dots(19)$$

then with

$$q_i^{(R)} = \delta r_i / (\delta r_i + \delta r_{i-1}) \quad \dots(20)$$

we obtain

$$\begin{aligned}
-\int_{ij} G \omega dS &= w_{ij}^{(Z)} \left[\left(1 - q_j^{(Z)}\right) \omega_{ij} + q_j^{(Z)} \omega_{ij-1} \right] - \\
&- w_{ij+1}^{(Z)} \left[\left(1 - q_{j+1}^{(Z)}\right) \omega_{ij+1} + q_{j+1}^{(Z)} \omega_{ij} \right] + \\
&+ w_{ij}^{(R)} \left[\left(1 - q_i^{(R)}\right) \omega_{ij} + q_i^{(R)} \omega_{i-1,j} \right] - \\
&- w_{i+1,j}^{(R)} \left[\left(1 - q_{i+1}^{(R)}\right) \omega_{i+1,j} + q_{i+1}^{(R)} \omega_{ij} \right]. \quad \dots (21)
\end{aligned}$$

Using mass conservation,

$$w_{ij}^{(Z)} + w_{ij}^{(R)} - w_{ij+1}^{(Z)} - w_{i+1,j}^{(R)} = 0 \quad \dots (22)$$

and equation 21 can be cast in the more convenient form

$$\begin{aligned}
-\int_{ij} G \omega dS &= w_{ij}^{(Z)} q_j^{(Z)} (\omega_{i,j-1} - \omega_{ij}) \\
&- w_{ij+1}^{(Z)} (1 - q_{j+1}^{(Z)}) (\omega_{i,j+1} - \omega_{ij}) \\
&+ w_{ij}^{(R)} q_i^{(R)} (\omega_{i-1,j} - \omega_{ij}) \\
&- w_{i+1,j}^{(R)} (1 - q_{i+1}^{(R)}) (\omega_{i+1,j} - \omega_{ij}) \quad \dots (23)
\end{aligned}$$

This equation gives the convective flow of the desired species into a volume element located away from boundary surfaces. Boundary intervals are considered in section 3.5.

3.3 Concentration Diffusion

The concentration diffusion current across surface $A_{i,j}^{(Z)}$ is approximated, from equation 15, by

$$\begin{aligned}
C_{ij}^{(Z)} &= A_{ij}^{(Z)} \left[\frac{\omega_{i,j-1} - \omega}{\delta z_{j-1} / (2\eta_{i,j-1})} \right] = A_{ij}^{(Z)} \left[\frac{\omega - \omega_{i,j}}{\delta z_j / (2\eta_{ij})} \right] \\
&= 2A_{i,j}^{(Z)} \left[\frac{\omega_{i,j-1} - \omega_{i,j}}{(\delta z_{j-1} / \eta_{i,j-1}) + (\delta z_j / \eta_{i,j})} \right] \quad \dots (24)
\end{aligned}$$

where ω is an interpolated concentration of surface $A_{i,j-1}^{(Z)}$. The total concentration diffusion current into volume interval i,j , is

$$\int \eta \cdot \nabla \omega \cdot dS = C_{i,j}^{(Z)} - C_{i,j+1}^{(Z)} + C_{i,j}^{(R)} - C_{i+1,j}^{(R)}$$

$$\begin{aligned}
&= C_{ij}^{(Z)} (\omega_{i,j-1} - \omega_{ij}) + C_{i,j-1}^{(Z)} (\omega_{i,j+1} - \omega_{i,j}) \\
&+ C_{ij}^{(R)} (\omega_{i-1,j} - \omega_{ij}) + C_{i+1,j}^{(R)} (\omega_{i+1,j} - \omega_{i,j}) \quad \dots (25)
\end{aligned}$$

where,

$$C_{ij}^{(Z)} = 2A_{ij}^{(Z)} / (\delta z_{j-1} / \eta_{i,j-1} + \delta z_j / \eta_{ij}) \quad \dots (26)$$

and

$$C_{ij}^{(R)} = 2A_{ij}^{(R)} / (\delta x_{i-1} / \eta_{i-1,j} + \delta x_i / \eta_{i,j}) \quad \dots (27)$$

Boundary terms in equation 25 will be considered after expressions have been generated for pressure diffusion.

3.4 Pressure Diffusion

The pressure diffusion current across surface $A_{ij}^{(Z)}$ is approximated, from equation 15, by

$$\begin{aligned}
P_{ij}^{(Z)} &= A_{ij}^{(Z)} \cdot \frac{\ln P_{ij-1} - \ln P}{\Omega_{i,j-1}^{(Z)}} = A_{ij}^{(Z)} \frac{\ln P - \ln P_{ij}}{\Omega_{ij}^{(Z)}} \\
&= A_{ij}^{(Z)} \frac{\ln(P_{ij-1}/P_{ij})}{\Omega_{ij-1}^{(Z)} + \Omega_{ij}^{(Z)}} \quad \dots (28)
\end{aligned}$$

where P is an interpolated pressure at $A_{ij}^{(Z)}$ and

$$\Omega_{ij}^{(Z)} = \delta z_j / \left[2\eta \frac{D}{D} \cdot \frac{\Delta M}{M} \omega(1-\omega) \right]_{ij} \quad \dots (29)$$

Similarly, the pressure diffusion current across surface $A_{ij}^{(R)}$ is:

$$P_{ij}^{(R)} = A_{ij}^{(R)} \cdot \frac{\ln(P_{i-1,j}/P_{i,j})}{\Omega_{i-1,j}^{(R)} + \Omega_{ij}^{(R)}} \quad \dots (30)$$

where

$$\Omega_{ij}^{(R)} = \delta x_i / \left[2\eta \frac{D}{D} \frac{\Delta M}{M} \omega(1-\omega) \right]_{ij} \quad \dots (31)$$

The total pressure diffusion current into volume interval i,j is:

$$\int_{ij} \eta \cdot \frac{D}{D} \cdot \frac{\Delta M}{M} \cdot \omega(1-\omega) \nabla \ln P \, dS = S_{i,j}$$

$$S_{ij} = P_{i,j}^{(Z)} - P_{i,j+1}^{(Z)} + P_{i,j}^{(R)} - P_{i+1,j}^{(R)} \quad \dots (32)$$

For elements adjacent to boundaries, it is assumed that the nett diffusion from both pressure and concentration effect, is zero across the boundary surface. For example, if element $i,j-1$ is outside the boundary whilst i,j is inside, then

$$C_{i,j}^{(Z)} (\omega_{i,j-1} - \omega_{i,j}) + P_{i,j}^{(Z)} = 0 \quad \dots(33)$$

3.5 Boundary Conditions

In sections 3.2, 3.3 and 3.4 above, volume intervals located away from boundary surfaces have been considered. For an interval adjacent to a solid boundary surface, the convective flow across that boundary must be zero, as must diffusion from both pressure and concentration effects. Hence the relevant terms in equations 23, 25, 32 are set to zero. For positive outflow, it is assumed that ω outside the boundary is equal to that just inside. In addition, pressure diffusion across the boundary can be ignored and the relevant terms in equations 23, 25 and 32 can be discarded. For positive inflow, the convective flow of desired species, $W_{in} \cdot \omega_{in}$ is usually known at a large distance from the boundary where mass diffusion can be neglected. At the boundary, the total flow of desired species must also equal $W_{in} \cdot \omega_{in}$ but because of the possibility of mass diffusion across the boundary, the concentration at the boundary will not necessarily equal ω_{in} . This does not affect the application of the boundary condition (that the total flow of desired species equals $W_{in} \cdot \omega_{in}$) which is accounted for by setting the concentration and pressure diffusion terms to zero and the convective flow equal to $W_{in} \cdot \omega_{in}$. The appropriate term of equation 23 then becomes $W_{in} (\omega_{in} - \omega_{i,j})$.

3.6 Mass Balance for Volume Interval

Collecting the various terms for flow of the desired species into volume element i,j we have from equations 15, 23, 25 and 32

$$\begin{aligned} & W_{i,j}^{(Z)} \cdot q_j^{(Z)} (\omega_{i,j-1} - \omega_{i,j}) - W_{i,j+1}^{(Z)} (1-q_{j+1}^{(Z)}) (\omega_{i,j+1} - \omega_{i,j}) + \\ & + W_{i,j}^{(R)} \cdot q_i^{(R)} (\omega_{i-1,j} - \omega_{i,j}) - W_{i+1,j}^{(R)} (1-q_{i+1}^{(R)}) (\omega_{i+1,j} - \omega_{i,j}) + \\ & + C_{i,j}^{(Z)} (\omega_{i,j-1} - \omega_{i,j}) + C_{i,j+1}^{(Z)} (\omega_{i,j+1} - \omega_{i,j}) + \\ & + C_{i,j}^{(R)} (\omega_{i-1,j} - \omega_{i,j}) + C_{i+1,j}^{(R)} (\omega_{i+1,j} - \omega_{i,j}) + \\ & + S_{i,j} = 0 \quad \dots(34) \end{aligned}$$

Define

$$h_{i,j}^{(Z-)} = C_{i,j}^{(Z)} + W_{i,j}^{(Z)} q_j^{(Z)} \quad \dots (35)$$

$$h_{i,j}^{(Z+)} = C_{i,j+1}^{(Z)} - W_{i,j+1}^{(Z)} (1-q_{j+1}^{(Z)}) \quad \dots (36)$$

$$h_{i,j}^{(R-)} = C_{i,j}^{(R)} + W_{i,j}^{(R)} q_i^{(R)} \quad \dots (37)$$

$$h_{i,j}^{(R+)} = C_{i+1,j}^{(R)} - W_{i+1,j}^{(R)} (1-q_{i+1}^{(R)}) \quad \dots (38)$$

Then

$$\begin{aligned} \omega_{i,j} (\sum h) = S_{i,j} + h_{i,j}^{(Z-)} \cdot \omega_{i,j-1} + h_{i,j}^{(Z+)} \omega_{i,j+1} + h_{i,j}^{(R-)} \omega_{i-1,j} + \\ + h_{i,j}^{(R+)} \omega_{i+1,j} \quad \dots (39) \end{aligned}$$

3.7 Iterative Solution of Finite Difference Equations

The non-linear dependence of $S_{i,j}$ and $\omega_{i,j}$ and its neighbouring ω 's suggests an iterative scheme to obtain a solution. An initial guess of the concentration (ω) field allows the S field to be calculated from equation 32 (using equations 28 to 31) then a new ω field can be calculated using the linear equation 39 for each volume interval.

In general, the number of volume intervals will be too large to contemplate a direct solution of equation 39 so an inner iterative loop is required with an outer iteration loop working on $S_{i,j}$. For the non-symmetric matrix involved in the inner loop, the extrapolated successive iteration method (Lee and Stone 1959) has been applied. This method is convergent provided that the h 's of equations 35 to 38 are positive. From equations 26 and 27, it is noted that the C 's are positive hence it is required that:

$$C_{i,j}^{(Z)} > |W_{i,j}^{(Z)}| \cdot (q_j^{(Z)} \text{ or } 1-q_j^{(Z)}) \quad \dots (40)$$

$$\text{and } C_{i,j}^{(R)} > |W_{i,j}^{(R)}| \cdot (q_i^{(R)} \text{ or } 1-q_i^{(R)}) \quad \dots (41)$$

depending on the flow direction.

Substituting for the q 's from equations 19 and 20 and for the C 's from equations 26 and 27 and ignoring any small differences between η_{ij} and its neighbours, we obtain the convergence criteria:

$$(\delta z_j \text{ or } \delta z_{j-1}) < \frac{2\eta_{ij}}{|W_{ij}^{(Z)}/A_{ij}^{(Z)}|} = 2\eta_{i,j} |G_{i,j}^{(Z)}| \quad \dots (42)$$

and

$$(\delta r_i \text{ or } \delta r_{i-1}) < \frac{2\eta_{ij}}{|w_{ij}^{(R)}/A_{ij}^{(R)}|} = 2\eta_{ij} |G_{ij}^{(R)}| \quad \dots(43)$$

where the G's are mass fluxes.

The extrapolated successive iteration method requires an acceleration parameter, the ω in equation 3.16 of Lee and Stone (1959), $\omega=1$ gives unaccelerated successive iteration. It was found that a value of ω of between 1.5 and 1.7 has halved the number of iterations required for problems so far attempted.

4. THE COMPUTER PROGRAMME TWIST

The computer programme TWIST has been developed to solve the equations derived in the previous sections. A FORTRAN IV listing is given in Appendix C.

4.1 Input Data

The necessary input data for the TWIST4 version are detailed in Appendix B. It should be noted that these must be expressed in dimensionless form in terms of the characteristic variables as defined in Section 2.

4.2 Convergence Problems

Initial difficulties associated with the stability of the programme have been overcome to some extent by adopting a more flexible programming philosophy. It was found necessary at an early stage to build in procedures to check the convergence or otherwise of both the inner and outer iteration loops, to terminate the programme if there was no convergence. This did not prove to be as simple as expected as an initial fluctuation must be permitted due to the arbitrary nature of the initial guess at the concentration field. Also, convergence to a requested accuracy may not be possible due to the quasi-stationary nature of the solution when the 'final' value has been reached, where slight fluctuations may occur due to round off errors. The programme will terminate after 10 successive divergences in either the inner or outer iteration loops.

4.3 Switching Between Iteration Loops

The optimum point at which to switch between the inner and outer iteration loops will depend on how strongly the coefficients determined in the outer loop depend on the parameter determined in the inner loop. Two alternatives have been made available in TWIST4. The user may specify the number of inner and outer loops to be traversed after which the programme will terminate. The default option will proceed with the inner loop iteration either until the convergence has reached the required accuracy or until the convergence (change in concentration between successive iterations) is less than 10% of the

maximum change between the first and second iterations of the loop, whichever occurs first. The programme will then return to the outer loop to recalculate coefficients. These criteria reduce significantly the computer time involved in reaching the final solution. In addition the programme will return to the outer loop immediately if there is a concentration change of 50% or more between successive iterations.

4.4 Problem Size

To alleviate problems caused by the small mesh intervals required when large flows are involved, the overall mesh size has been made flexible within the limits of $IMAX * JMAX = 2000$ rather than having a fixed size in either direction.

$IMAX$ = number of points in the radial direction

$JMAX$ = number of points in the axial direction.

5. COMPARISON WITH COHEN'S THEORY FOR THE COUNTER-CURRENT CENTRIFUGE

A flow distribution which could be readily treated by both TWIST and by Cohen's centrifuge theory was

$$G_z = \begin{cases} +g, 0 < r < r_i \\ -g, r_i < r < r_o \end{cases} \quad g \text{ constant}$$

where G_z is the axial mass flux and r_o the outer radius of the device. The relative proportions of product and re-circulating flow can be varied by changing r_i .

Appendix A gives the equations resulting when Cohen's theory is applied to such a flow distribution. To compare TWIST to this theory, the enricher end of the centrifuge is isolated and our parameters chosen as,

$$r_o = 3.87 \quad , \quad z = 30$$

and

$$ar_o^2 = \frac{\Delta MV^2}{RT} = 0.2 \quad ,$$

V being the peripheral velocity.

The case of complete recirculation (zero product flow) was chosen with down flow L set at the optimum value of equation A15. For our selected value of r_o , this is $L = 55.335$.

For numerical stability, TWIST requires a mesh increment

$$\delta z < 2/g = \frac{2\pi r_o^2}{L} = 2r_o \sqrt{\left[\frac{2 \ln 2 - 1}{8} \right]}$$

or $\delta z < 1.7$ for our selected value of r_0 .

Choosing 20 axial mesh intervals, with $\delta z = 1.5$, we have more than enough for accuracy, but a basic difficulty of the TWIST method is revealed, for larger flows would require a proportionately larger number of mesh points, and realistic centrifuges could have flows which are an order of magnitude greater than L_{opt} , making data preparation tedious and lengthening computer time.

In the radial direction, six annuli of equal flow area $A_{ij}^{(Z)}$ were chosen. Figure 2 shows the internal flow distribution, with the length of the smallest arrow being equal to $L/6$, that is 9.22. TWIST requires an inflow with concentration defined at at least one point, so a small through flow of magnitude 0.01 had to be imposed and added to the flows in the centre core. An extra axial mesh interval was needed for definition of the feed concentration which was taken as 0.007.

For the particular problem under consideration, Cohen's theory (equation A16) gives a separation factor of 1.554. The computed concentration profile from TWIST is plotted in Figure 3. Although the concentration profile itself has converged, the level has not. This was evident from the outflow concentration which should have converged to that of the feed stream. The lack of convergence produced mass balance errors of the same order of magnitude as the feed flow of the desired isotope. However, no convergence difficulties were experienced with more realistic feed flows.

The maximum separation factor calculated by TWIST was 1.576. This included radial separation which was neglected in Cohen's axial separation factor. The TWIST axial separation factor varied from 1.478 at the inner core to 1.501 at the outer annulus.

This good agreement shows that results from the code are valid for this type of device. Further comparisons of the code with experimental measurements would be an advantage.

6. CONCLUSIONS

The computer programme TWIST is available for the solution of pressure-diffusion problems describable in an R-Z coordinate system. The programme would be particularly suited to the analysis of separation in vortex tube devices with their complex secondary flow patterns, but also has application to the counter-current centrifuge, if only to validate the results of simpler theories. Such an application has indeed confirmed the result of Cohen's theory for the case of complete re-circulation.

The particular numerical technique used in TWIST was chosen so that mass is conserved irrespective of the coarseness of subdivision of the system volume.

However, for numerical stability, the method is found to require a very fine subdivision of the system volume when the internal mass flux is large. Its applicability to realistic counter-current centrifuges is doubtful.

For problems with realistic throughput (feed, product and waste mass flows) no severe convergence problems arise. Typically, each outer loop requires several hundred inner iterations and some five to ten outer loops are needed. The concentration level itself is slow to converge for problems with small mass throughput, but this is understandable in terms of round off errors and is of little consequence.

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8. NOTATION

(Notation is as follows except where otherwise defined in the text).

A	Lighter component of binary gas mixture.
$A_{ij}^{(R)}$	Area in radial direction of interval ij defined by equation 17.
$A_{ij}^{(Z)}$	Area in axial direction of interval ij defined by equation 16.
A^*	Characteristic area (multiple of $(L^*)^2$).
B	Heavier component of binary gas mixture.
$C_{ij}^{(R)}$	Coefficient defined by equation 27.
$C_{ij}^{(Z)}$	Coefficient defined by equation 26.
$C_{ij}^{(R)}$	Concentration diffusion current across surface $A_{ij}^{(R)}$.
$C_{ij}^{(Z)}$	Concentration diffusion current across surface $A_{ij}^{(Z)}$.
c	Molar density.
D	Diffusion coefficient.
D	Mass diffusivity.
G	Mass flux.
\tilde{G}	Dimensionless mass flux (defined by equation 11).
$G_{ij}^{(R)}$	Radial mass flux at interval ij .

$G_{ij}^{(Z)}$	Axial mass flux at interval ij .
G_Z	Axial mass flux.
$h_{ij}^{(R-)}$	Iteration coefficients for mass fractions as defined by equations 35 to 38.
$h_{ij}^{(R+)}$	
$h_{ij}^{(Z-)}$	
$h_{ij}^{(Z+)}$	
j_A	Mass flux of species A with respect to V
$j_A^{(c)}$	Concentration diffusion mass flux.
$j_A^{(p)}$	Pressure diffusion mass flux.
L^*	Characteristic length.
M	Mixture molecular weight.
M_A	Molecular weight of species A.
M_B	Molecular weight of species B.
P	Pressure.
P_{ij}	Pressure at interval ij .
$P_{ij}^{(R)}$	Pressure diffusion current across surface $A_{ij}^{(R)}$.
$P_{ij}^{(Z)}$	Pressure diffusion current across surface $A_{ij}^{(Z)}$.
$q_i^{(R)}$	Variables related to mesh intervals, as defined by equations 19 and 20.
$q_j^{(Z)}$	
R	Gas constant.
r	Radius
r_i	Radial coordinate of mesh line i .
r_o	Outer radius of device.
S	Surface
\tilde{S}	Dimensionless surface defined by equation 14.
S_{ij}	Total pressure diffusion current into volume interval ij .
T	Temperature.
V	Peripheral velocity.
v	mass averaged velocity.

$W_{ij}^{(R)}$	Mass flow rate in radial direction at interval ij .
$W_{ij}^{(Z)}$	Mass flow rate in axial direction at interval ij .
X_A	Mole fraction of species A.
Z	Length of device.
Z_j	Axial coordinate of mesh line j .
ΔM	Difference in molecular weights of species.
δr	Radial mesh interval.
δz	Axial mesh interval.
ρ	Mixture density.
ρ_A	Density of species A.
η	Defined by equation 12 to reflect temperature dependence of (ρD)
η_{ij}	Value of η applicable at interval ij .
ω_A	Mass fraction of species A.
ω	Interpolated mass fraction at surface $A_{ij-1}^{(Z)}$.
ω_{ij}	Mass fraction of species A at interval ij .
$\Omega_{ij}^{(R)}$	Variable defined by equation 31.
$\Omega_{ij}^{(Z)}$	Variable defined by equation 29.

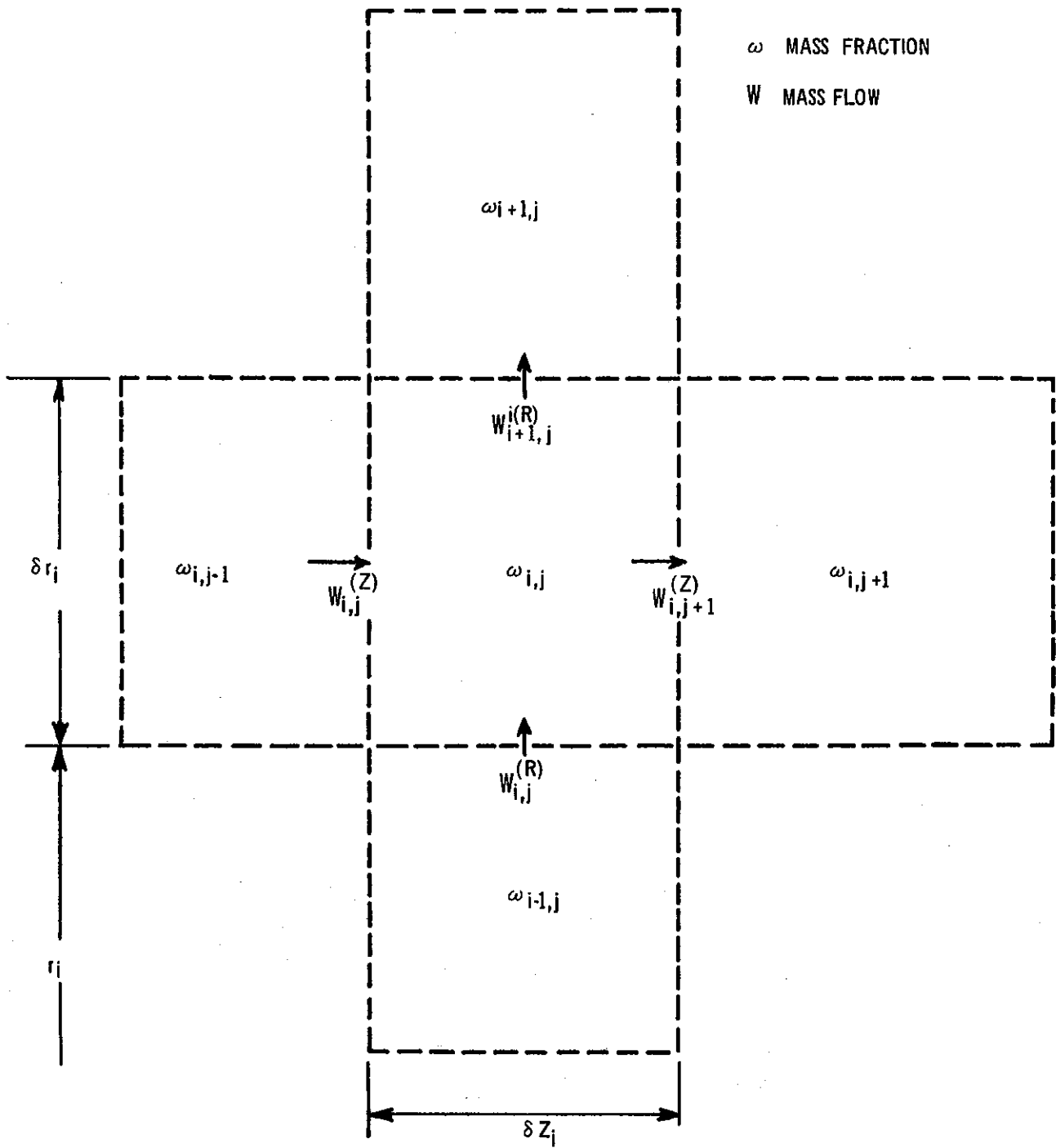


FIGURE 1. A FINITE VOLUME ELEMENT WITH NEIGHBOURS

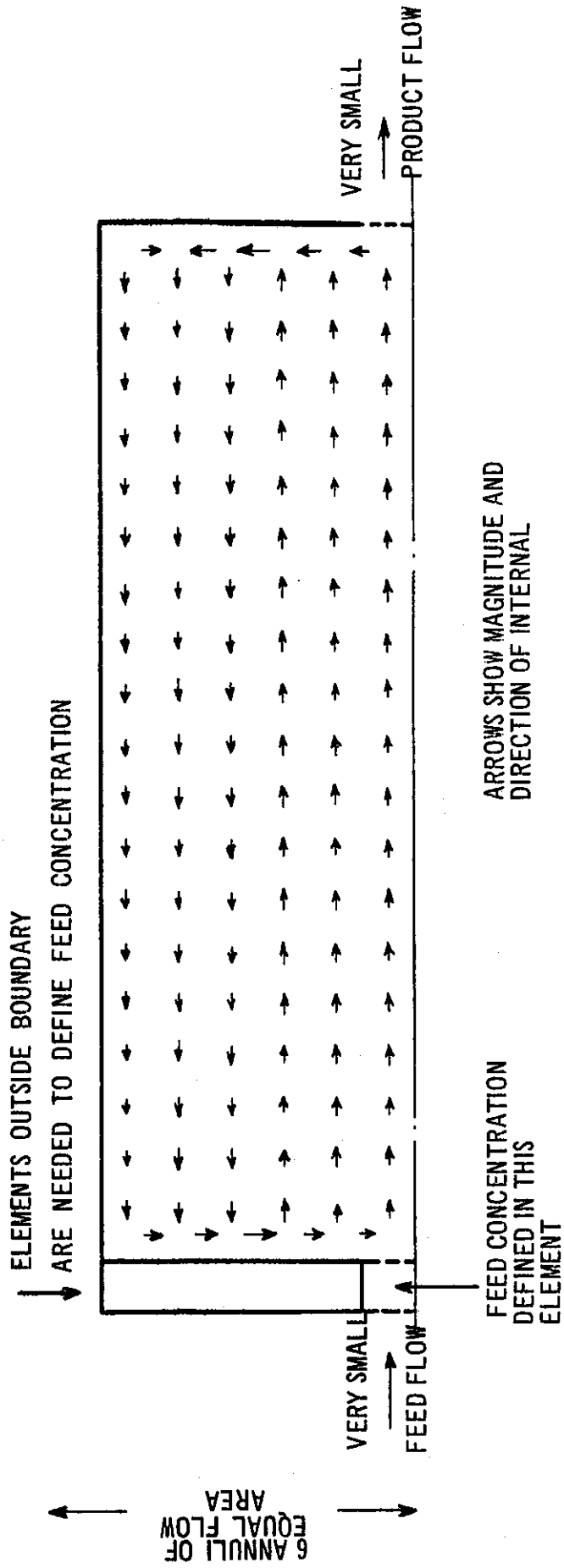


FIGURE 2. COUNTER-CURRENT FLOW DISTRIBUTION FOR TWIST



FIGURE 3. CONCENTRATION PROFILE FROM TWIST FOR COUNTER-CURRENT CENTRIFUGE

APPENDIX A

COHEN'S APPROACH FOR THE COUNTER-CURRENT CENTRIFUGE

By recognising that all length measurements are expressed in multiples of L^* and all mass fluxes are expressed as multiples of $(\rho.D)^*/L^*$, equation 10 can be written without the *tilda* as:

$$\nabla.G\omega = \nabla.(\eta\nabla\omega + \eta \frac{D}{D} \cdot \frac{\Delta M}{M} \cdot \omega (1-\omega) \nabla.\ln P) \quad \dots A1$$

For zero radial flow, zero axial pressure gradient, uniform temperature ($\eta = 1$), $D = D$ and $\omega \ll 1$, this equation reduces to:

$$G_Z \frac{\partial \omega}{\partial z} = \frac{\partial^2 \omega}{\partial z^2} + \frac{1}{r} \frac{\partial}{\partial r} \cdot r \left[\frac{\partial \omega}{\partial r} + \frac{\Delta M}{M} \cdot \omega \cdot \frac{\partial \ln P}{\partial r} \right] \quad \dots A2$$

Taking the radial pressure distribution as that for a solid body,

$$G_Z \cdot \frac{\partial \omega}{\partial z} = \frac{\partial^2 \omega}{\partial z^2} + \frac{1}{r} \frac{\partial}{\partial r} \cdot r \left[\frac{\partial \omega}{\partial r} + a.r.\omega \right] \quad \dots A3$$

where

$$a = \frac{\Delta M \cdot (\Omega L^*)^2}{RT} \quad \dots A4$$

with due regard to the dimensionless form of equation A3 it is the same as Cohen's equation 6.45. Using his method of eliminating the r dependence of ω we obtain the simplification:

$$(c_2 + c_3) \frac{d\omega}{dz} - (P + c_1) \omega = -P\omega_p \quad \dots A5$$

where

$$c_1 = a \int_0^{r_0} r \int_0^r G_Z \cdot 2\pi r' dr' dr \quad \dots A6$$

$$c_2 = \pi r_0^2 \quad \dots A7$$

$$\text{and } c_3 = \int_0^{r_0} r^{-1} \left[\int_0^r G_Z \cdot 2\pi r' dr' \right]^2 dr / 2\pi \quad \dots A8$$

where ω_p is the concentration at the product end and P is the product flow (in multiples of $(\rho D)^* L^*$). Consider the flow distribution

$$G_Z = \begin{cases} +g, & 0 < r < r_1 \\ -g, & r_1 < r < r_0 \end{cases} \quad g \text{ constant} \quad \dots A9$$

The total up and down flow is

$$L = \pi r_o^2 g \quad \dots A10$$

and the product flow

$$P = \pi g [2r_i^2 - r_o^2] \quad \dots A11$$

is varied by changing r_i .

In terms of L and P, equations A6 and A8 yield

$$c_1 = a \cdot \frac{r_o^2}{8} \cdot \frac{L^2 + 2PL - P^2}{L} \quad \dots A12$$

and

$$c_3 = \frac{1}{2\pi} \left\{ \frac{2P^2 - L^2}{4} + \frac{(P+L)^2}{2} \cdot \ln \left(\frac{2L}{P+L} \right) \right\} \quad \dots A13$$

The solution to equation A5 is, for the enricher end of the centrifuge,

$$\alpha = \frac{\omega_P}{\omega_F} = (P+c_1) / \left[P+c_1 \cdot \exp \left(- \frac{P+c_1}{c_2+c_3} \cdot Z \right) \right] \quad \dots A14$$

where ω_F is the feed concentration and Z is the enricher length. By allowing negative L, equation A14 is also valid for the stripper, in which case P would denote the waste rather than product flow.

At zero production, α is stationary when

$$L = L_{opt} = \pm \pi r_o \sqrt{\left[\frac{8}{2 \cdot \ln 2 - 1} \right]} \quad \dots A15$$

The positive result gives the optimum enricher flow and the negative result gives the optimum stripper flow. The maximum separation factor is

$$\alpha_{max} = \exp \left(\frac{a \cdot r_o \cdot Z}{16} \right) \sqrt{\left[\frac{8}{2 \cdot \ln 2 - 1} \right]} \quad \dots A16$$

APPENDIX B

PREPARATION OF INPUT DATA FOR TWIST4

1. INPUT DATA FOR TWIST4

Card 1: (Format 20A4) }
Card 2: (Format 20A4) } Title cards to describe the run.
Card 3: (Format I3)

NC Number of cases to be processed (programme terminates
 when NC becomes zero).

2. FIRST CASE SPECIFICATION

Card 4: (Format 3I3,6E10.0)

IMAX,JMAX Number of Radial and Axial mesh spaces.
 (Maximum problem size $IMAX \cdot JMAX = 2000$).

NBF Number of points at which concentration is to be
 defined. (Must be at least 1).

AM,BM Molecular weights of species A and B with respect to
 characteristic mixture mean, (species A being the
 lighter). (Must be non-zero, and unequal.)

AREA Characteristic area A^* as a multiple of (characteris-
 tic length, L^*)².

RD Ratio D/D (must be non-zero), normally = 1.0.

ACC Accuracy for the final iteration of the inner and
 outer loops. (Maximum variation in concentration
 between successive iterations.) This figure will be
 used to terminate the iteration if NINNER and NOUTER
 are not specified on the next card.

GUESS Guess at concentration for all undefined internal
 points (must not be zero or 1.0). This figure is not
 required for cases when a variable initial guess is to
 be made (see card 16) or when restarting a case from
 punched cards (NPUNCH=2).

Card 5: (Format 4I3,2E10.0)

NPUNCH To determine punched card outputs.
 NPUNCH=0, No punched card output.
 NPUNCH=1, Punched card output of final concentration
 field.

 NPUNCH=2, For case being restarted with punched cards
 from previous run.

NINNER \neq 0 Number of iterations for inner loop.

- $N_{OUTER} \neq 0$ Number of iterations for outer loop.
- W Acceleration coefficient.
 Usually $1.0 \leq W \leq 2.0$, the default option being $W=1.5$.
- Card 6: (Format 36I2)
- N(I,J) Boundary specification for all elements.
 N=0 for elements outside the boundary.
 N=1 for elements inside the boundary.
- Card 7: (Format 2I3, E10.0)
- I,J,F(I,J) There will be NBF cards in this set (i.e. at least one) as specified on Card 2.
 The concentration, F, is specified for point (I,J) for which N(I,J) must equal 0 ($F(I,J) \neq 0$ or 1).
- Card 8: (Format I3)
- IN To determine the method of reading in the radial mesh.
 IN=1, Read in mesh in Format (E6.0,I3) as cards 9a.
 IN \neq 1, Read in mesh spaces individually as cards 9b.
- Cards 9a: (Format E6.0,I3)
- DR(I),N Indicates N radial mesh spaces of width DR(I). A new card is required for each change in mesh width until $\sum(N)=IMAX$. DR(I) must be a multiple of the chosen characteristic length, L*.
- Cards 9b: (Format 12E6.0)
- DR(I) Radial mesh spacing for each interval as a multiple of characteristic length, L*.
- Card 10: (Format I3)
- IN (To determine the method of reading in the axial mesh, cards 11a or 11b. (Similar to card 8 for radial mesh).
- Cards 11a: (Format E6.0,I3)
- DZ(I),N Indicates N axial mesh spaces of width DZ(I) similar to cards 9a for the radial mesh.
- Cards 11b: (Format 12E6.0)
- DZ(J) Axial mesh spacing for each interval as a multiple of characteristic length, L*.
- Cards 12: (Format 12E6.0)
- P(I,J) Relative Pressure field. (New card required for each change in axial position.)
- Card 13: (Format I3)
- ITEMP To determine the temperature field.

ITEMP=1 read in an eta field on cards 14

ITEMP≠1 assume a uniform eta field, next cards type 15.

Cards 14: (Format 12E6.0)

T(I,J) Eta field referred to characteristic eta.
(New card required for each change in axial position.)

Cards 15: (Format (3X,11E6.0)/12E6.0...)

WZ(1,1) . . .
WR(1,1) WR(2,1) . . . Flow field
WZ(1,2) . . .
.

The flow field is input with axial and radial elements on alternate lines.
Due regard must be taken of mass conservation requirements.

Flows are calculated with respect to $A*(\delta D)^*/L^*$.

Card 16A: (Format I3)

(If NPUNCH.EQ.2 only cards 16C are required)

KZ Determines guess for initial concentration iteration.
KZ=0 will set all non defined concentrations=GUESS.
KZ=1 will read in a variable guess (see cards 16B).
KZ=∅ or 1 programme terminates.

Cards 16B: (Format 12E6.0)

F(I,J) Initial guess at concentration for all points (I,J),
including specified points (only if KZ=1 on card 14,
otherwise omit these cards).

Cards 16C: (Format 6E12.5)

(only used if NPUNCH.EQ.2)

F(I,J) Initial guess at concentration field for all points.
Read in punched cards as output from the previous run.

3. CHANGE OF DATA FOR NEXT CASE

(Provided NC was specified as greater than 1)

Card 18: (Format I3)

NCHTP Type of data change for next case.
NCHTP less than zero, programme terminates.
NCHTP=0 all data to be changed, requires a new set of
cards 4 to 17.
NCHTP=1 a few data items to be changed in the same
problem geometry (see card 19 et sequens).

Card 19: (Format 2I3)

NN Specifies which items are to be changed as follows:

NN=-3 change entire flow field but no other items.
 NN=-2 change some values of flow field and some P, T,
 or molecular weights.

NN=-1 change some P, T, or molecular weights.

NN=0 change some items in flow field but no other
 items.

NN=+1 change accuracy or acceleration scheme, but no
 other items.

NN=+2 change pressure field but no other items.

NN=+3 change eta field but no other items.

NM

Total number of changes to flow, eta and pressure
 fields (options NN=-2, -1 and 0 only).

(N.B. In option NN=-2, NM is number of items to be
 changed in flow field and number of items in eta +
 pressure.)

If more complex data changes are required it is recommended that the
 facility NCHTP=0 be used on CARD 18.

Cards 20

NN=-3

New set of cards 15.

NN=-2

(i) Namelist, changes in molwts AM or BM using
 namelist e.g. ~~MOLWT~~AM=1.001 \$END.

(ii) Changes in Pressure or temp using Format
 (A1,2(LX,I3), 2X,E13.6)

e.g. P(I,J) = +1.005071E+00

T(I,J) = +0.999999E+00

(iii) For changes in flow field Format
 (A2,2(LX,I3), 2X,E13.6)

e.g. WZ(I,J)=+1.000000E+00

(iv) Changes in iteration scheme use namelist \$NEWACC
 for any of items ACC,W,ALAMAX,ALAMIN,NSPEED.

NN=-1

As for items (i) and (ii) of NN=-2

NN=0

As for item (iii) of NN=-2

NN=+1

As for item (iv) of NN=-2

NN=+2

New set of cards 12

NN=+3

New set of cards 14.

APPENDIX C

PROGRAMME LISTING

C		10
C	MAINLINE	20
C		30
C	1*IST FOUR	40
C		50
	DIMENSION CR(2000),CZ(2000),GR(2000),QZ(2000),AR(2000),AZ(2000),	60
	IP(2000),T(2000),F(2000),FM1(2000),FP1(2000),FF(2000),HL(2000),	70
	2*HR(2000),HL(2000),HD(2000),SUM(2000),S(2000)	80
	DIMENSION CR(2001),DZ(2001)	90
	DIMENSION N(2002)	100
	DIMENSION WR(2004),WZ(2004),NS(2004)	110
	READ(1,2000) IMAX,JMAX	120
	IMP1=IMAX+1	130
	IMP2=IMAX+2	140
	JMP1=JMAX+1	150
	JMP2=JMAX+2	160
	CALL MAIN2 (CR,CZ,GR,CZ,AR,AZ,P,T,F,FM1,FP1,FF,HL,HR,HU,HD,SUM,S,	170
	3*DR,DZ,N,WR,WZ,NS,IMAX,JMAX,IMP1,IMP2,JMP1,JMP2)	180
	2000 FCFMAT(213)	190
	END	200
	SUBROUTINE MAIN2 (CR,CZ,GR,QZ,AR,AZ,P,T,F,FM1,FP1,FF,HL,HR,HU,HD,	210
	1,SUM,S,DR,DZ,N,WR,WZ,NS,IMAX,JMAX,IIMP1,IIMP2,JJMP1,JJMP2)	220
C	MAINLINE INPUT DATA: NC, NCHTP	230
C	NC=NO. OF CASES TO PRECESS	240
C	NCHTP=TYPE OF DATA CHANGE FOR NEXT CASE.	250
C	NCHTP=0, CHANGE ALL DATA.	260
C	NCHTP=1, CHANGE A FEW ITEMS (SEE SUBROUTINE DATACH).	270
C		280
	COMMON /AREA/ AREA	290
	COMMON /GUESS/ GUESS	300
	COMMON /MCLATS/ AM,BM	310
	COMMON /NBF/ ABF	320
	COMMON /PUNCH/ NPUNCH	330
	COMMON /LAMBDA/ ALAMAX,ALAMIN	340
	COMMON /LIMITS/ IMP1,IMP2,JMP1,JMP2	350
	COMMON /ACC/ ACC,EMAX1,ALPHA,BETA,NJ,W,NSPEED,NINNER,ROUTER	360
	COMMON /CCNVRG/ CCNVI,KK	370
		380
	IMP1=IIMP1	390
	IMP2=IIMP2	400
	JMP1=JJMP1	410
	JMP2=JJMP2	420
	DIMENSION CR(IMP1),DZ(JMP1)	430
	DIMENSION WR(IMP2,JMP2),WZ(IMP2,JMP2)	440
	DIMENSION P(IMAX,JMAX),T(IMAX,JMAX)	450
	DIMENSION F(IMAX,JMAX),FM1(IMAX,JMAX),FP1(IMAX,JMAX)	460

DIMENSION N(IMP1, JMP1)	470
DIMENSION AR(IMAX, JMAX), AZ(JMAX)	480
DIMENSION CR(IMAX), CZ(JMAX)	490
DIMENSION CR(IMAX, JMAX), CZ(IMAX, JMAX)	500
DIMENSION FF(IMAX, JMAX)	510
DIMENSION NS(IMP2, JMP2)	520
DIMENSION S(IMAX, JMAX)	530
DIMENSION HL(IMAX, JMAX), HR(IMAX, JMAX), HU(IMAX, JMAX),	540
HC(IMAX, JMAX), SUM(IMAX, JMAX)	550
DIMENSION CHAR(40)	560
READ(1, 2001)(CHAR(I), I=1, 40)	570
WRITE(3, 2001)(CHAR(I), I=1, 40)	580
NN=0	590
NK=0	600
NJ=0	610
KK=0	620
READ(1, 2000) NC	630
WRITE(3, 3000) NC	640
IF(NC.LE.0) GO TO 1000	650
1001 CALL CASFIN(F, FM1, FP1, WR, WZ, DR, DZ, P, T, RD, ALAMAX	660
, ALAMIN, NS, IMAX, JMAX, IMP1, IMP2, JMP1, JMP2)	670
CALL IDNTFY(N, NS, IMAX, JMAX, IMP1, IMP2, JMP1, JMP2)	680
CALL INLSFT(F, FM1, FF, NS, IMAX, JMAX)	690
CALL FEDEF(AR, AZ, DR, DZ, CR, CZ, R, IMAX, JMAX)	700
CALL CDIFF(CR, CZ, AR, AZ, DR, DZ, T, NS, IMAX, JMAX, C3, C4)	710
1002 CALL PDIFF(F, AR, AZ, S, P, T, RC, DR, DZ, NS, IMAX, JMAX, U3, U4, UR, UZ)	720
1003 CALL ILPREP(WR, WZ, CR, CZ, CR, CZ, HL, HR, HU, HC, SUM, IMAX, JMAX)	730
1004 CALL INLOCP(F, FM1, FP1, S, HL, HR, HU, HD, SUM, NS, IMAX, JMAX)	740
KK=KK+1	750
IF(NK.GE.NCUTER.AND.NCUTER.GE.1.AND.NINNER.GE.1) GO TO 1011	760
C	770
C IF NJ=1, INNER LOOP HAS GONE AS FAR AS POSSIBLE AND CAN ACHIEVE NO	780
C BETTER ACCURACY DUE TO ROUND OFF ERRORS, GO TO NEXT CASE.	790
C	800
IF(NJ.EQ.1) GO TO 1009	810
CALL MXCNCH(F, FF, IMAX, JMAX, CCNV2)	820
C	830
C CHECK IF OUTER LOOP DIVERGING.	840
C	850
IF(CONV2.GT.CCNV1) KK=KK+1	860
IF(KK.GT.10) GO TO 1005	870
CCNV1=CCNV2	880
C	890
C TEST IF BOTH INNER AND OUTER LOOPS SUFFICIENTLY CONVERGED.	900
C	910
IF(CONV2.LT.ACC.AND.EMAX1.LT.ACC) GO TO 1006	920
C	930
C OUTER LOOP NOT CONVERGED. PRINT PRESENT RESULT AND RETURN TO	940
C RECALCULATE COEFFICIENTS.	950
C	960
WRITE(3, 3001)	970
CALL FPRINT(F, IMAX, JMAX)	980
GO TO 1002	990
C	1000
C CASE CONVERGED, PRINT ANSWER.	1010
C	1020
1006 WRITE(3, 3002)	1030

WRITE(3,3001)	1040
CALL FPRINT(F,IMAX,JMAX)	1050
GO TO 1007	1060
1009 IF(W.SQ.1.C.AND.NSPEED.EQ.C) GO TO 1010	1070
NJ=0	1080
NSPEED=0	1090
WRITE(3,3005)	1100
CALL FPRINT(F,IMAX,JMAX)	1110
W=1.0	1120
GO TO 1002	1130
1010 WRITE(3,3004)	1140
CALL FPRINT(F,IMAX,JMAX)	1150
GO TO 1007	1160
1011 WRITE(3,3006)	1170
CALL FPRINT(F,IMAX,JMAX)	1180
GO TO 1007	1190
1005 WRITE(3,3003)	1200
CALL FPRINT(F,IMAX,JMAX)	1210
C	1220
C PREPARE FOR NEXT CASE.	1230
C	1240
1007 NC=NC-1	1250
IF(NPUNCH.EQ.1) CALL FPUNCH(F,IMAX,JMAX)	1260
WRITE(3,3000) NC	1270
IF(NC.LE.0) GO TO 1000	1280
FEAD(3,2000) NCHTP	1290
C	1300
C DETERMINE METHOD FOR CHANGING DATA FOR NEXT CASE.	1310
C	1320
KK=0	1330
IF(NCHTP)1000,1001,1008	1340
1008 CALL DATACH (NNA,P,T,PC,WR,WZ,NS,IMAX,JMAX)	1350
C	1360
C FROM TYPE OF DATA CHANGE MADE, DETERMINE WHERE TO RESTART PROBLEM.	1370
C	1380
IF(NNA.EQ.5) GO TO 1007	1390
IF(NNN) 1002,1003,1004	1400
1000 CONTINUE	1410
2000 FORMAT(I3)	1420
2001 FORMAT(20A4)	1430
3000 FORMAT('1','NO. OF CASES TO SOLVE=',I3)	1440
3001 FORMAT('0 CALCULATED CONCENTRATION FIELD',//)	1450
3002 FORMAT('0 OUTER LOOP CONVERGED')	1460
3003 FORMAT('0 OUTER ITERATION NOT CONVERGING. PROGRAMME TERMINATING.')	1470
3004 FORMAT('0 THIS CASE WILL NOT CONVERGE BEYOND PRESENT VALUES DUE TO 1 ROUND OFF ERRORS. PROCEEDING TO NEXT CASE.')	1480
3005 FORMAT('0 FURTHER CONVERGENCE IS INHIBITED BY ACCELERATION TECHNIQUE 1. '//, 'PROGRAMME WILL REVERT TO NON-ACCELERATED SCHEME TO ACHIEVE 2 FINAL RESULT.')	1490
3006 FORMAT('0 REQUESTED NUMBER OF OUTER LOOPS COMPLETED.')	1500
STOP	1530
END	1540
	1550

SUBROUTINE CASFIN (F,FM,FP,WP,WZ,DR,DZ,P,T,RD,ALAMAX,ALAMIN	1560
, NS,IMAX,JMAX,IMP1,IMP2,JMP1,JMP2)	1570
INPUT DATA FOR THIS CASE:	1580
CARD 1:(FORMAT 3I3,5F10.0)	1590
	1600
IMAX=NUMBER OF RADIAL MESH SPACES (1610
JMAX=NUMBER OF AXIAL MESH SPACES (IMAX*JMAX.LE.2000)	1620
NBF=NUMBER OF POINTS AT WHICH CONCENTRATIONS DEFINED (GE.1)	1630
AM=MOLECULAR WEIGHT OF SPECIES A (WRT MIXTURE MEAN)	1640
BM=MOLECULAR WEIGHT OF SPECIES B (WRT MIXTURE MEAN)	1650
AREA=CHARACTERISTIC AREA	1660
RD=(PRESSURE DIFFUSION COEFF)/(CONCENTRATION DIFFUSION COEFF)	1670
ACC=ACCURACY	1680
GUESS=GUESS AT CONCENTRATION FOR ALL UNKNOWN POINTS(NE.0.OR.1)	1690
	1700
CARD 2: FORMAT(3I3,2F10.0)	1710
	1720
NPUNCH=0 NO PUNCHED CARD INPUT OR OUTPUT	1730
NPUNCH=1 FOR PUNCHED OUTPUT OF FINAL CONCENTRATION FIELD	1740
NPUNCH=2 FOR CASE BEING RESTARTED WITH CARDS FROM PREVIOUS RUN	1750
	1760
	1770
	1780
NINNER = NUMBER OF ITERATIONS FOR INNER LOOP. (OPTIONAL)	1790
	1800
NOUTER = NUMBER OF ITERATIONS FOR OUTER LOOP. (OPTIONAL)	1810
	1820
	1830
W=ACCELERATION PARAMETER	1840
ZC=1.	1850
	1860
CARD SET 3:(FORMAT 24I3)	1870
N(I,J) I=1,IMAX;J=1,JMAX	1880
N=0 FOR VOLUME ELEMENTS OUTSIDE BOUNDARY	1890
N=1 FOR VOLUME ELEMENTS INSIDE BOUNDARY	1900
	1910
CARD SET 4:(FORMAT(2I3,E10.0))	1920
I,J,F(I,J)	1930
POINTS (I,J) AT WHICH CONCENTRATION IS DEFINED	1940
AND F(I,J) CONCENTRATION AT THIS POINT (NOT 0 OR 1)	1950
	1960
CARD 5:(FORMAT I3)	1970
IN, METHOD FOR READING IN RADIAL MESH	1980
IN=0, INPUT MESH AS CARDS 6A	1990
IN=1, INPUT MESH AS CARDS 6B	2000
	2010
CARD SET 6A:(FORMAT 12E6.C)	2020
DR(I) I=1,IMAX	2030
INDIVIDUAL RADIAL MESH SPACINGS (DIMENSIONLESS)	2040
	2050
CARD SET 6B:(FORMAT E6.0,I3)	2060
A,N DENOTES N MESH SPACES OF WIDTH A	2070
A NEW CARD IS REQUIRED FOR EACH CHANGE IN MESH WIDTH	2080
UNTIL SIGMA(N)=IMAX	2090
	2100
CARD 7:(FORMAT I3)	2110
IN, METHOD FOR READING IN AXIAL MESH (SEE CARD 5)	2120
	2130
ZB=0.5	2140
CARD SET 7A:(FORMAT 12E,0)	2150


```

CALL TRVIAL (RD,IMAX,JMAX)
C
C SET ALL CONCENTRATIONS F(I,J) TO ZERO
C SET ALL POINTS AS OUTSIDE PROBLEM BOUNDARY UNTIL SPECIFIED.
C
DO 1000 I=1,IMAX
DO 1000 J=1,JMAX
F(I,J)=0.0
NS(I+1,J+1)=0
1000 CONTINUE
CALL CONDEF (F,FMI,FP1,N,IMAX,JMAX)
CALL ACCTST (ACC)
C
C PRINT CONCENTRATION FOR EACH DEFINED POINT.
C
WRITE(3,3013)
WRITE(3,3002)
DO 1001 I=1,IMAX
DO 1001 J=1,JMAX
IF(F(I,J).NE.0) WRITE(3,3002) I,J,F(I,J)
1001 CONTINUE
C
C READ IN MESH SPACINGS DR,DZ
C
WRITE(3,3013)
WRITE(3,3004)
CALL MESHIN (DR,IMAX)
WRITE(3,3005)
CALL MESHIN (DZ,JMAX)
C
C READ IN PRESSURE & TEMPERATURE FIELDS.
C
WRITE(3,3006)
CALL FREAD (P,IMAX,JMAX,NS)
CALL FPRINT (P,IMAX,JMAX)
READ(1,2001) ITEM
IF(ITEM.EQ.1) GO TO 1005
WRITE(3,3014)
DO 1007 I=1,IMAX
DO 1007 J=1,JMAX
1007 T(I,J)=!.0
GO TO 1006
1005 WRITE(3,3007)
CALL FREAD (T,IMAX,JMAX,NS)
CALL FPRINT (T,IMAX,JMAX)
C
C READ IN FLOW FIELD AND PERFORM A MASS BALANCE CHECK.
C
1006 CALL FLOWIN (WR,WZ,IMAX,JMAX)
CALL FLWCHK (WR,WZ,IMAX,JMAX)
RETURN
1004 WRITE(3,3012)
STOP
C
2000 FORMAT(3I3,6E10.0)
2001 FORMAT(4I3,2E10.0)
3000 FORMAT(' ',' INPUT DATA ',//)
3001 FORMAT('0 ',' MESH SIZE ',I3, ' RADIAL *',I3, ' AXIAL ',//, ' NBF=',I3, /
1, ' AM=',1PE10.3, /' BM=',1PE10.3, /' AREA=',1PE10.3,
2 /, ' RD=',1PE10.3, /, ' ACC=',1PE10.3, /, ' GUESS=',1PE10.3//)
3002 FORMAT('0 SPECIFIED CONCENTRATIONS')

```

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```

3001 FORMAT('O POINT, I=',I3,2X,' J=',I3,3X,' CONC=',1PE10.3)
3002 FORMAT('O RADIAL MESH',/)
3003 FORMAT('O AXIAL MESH',/)
3004 FORMAT('O PRESSURE FIELD')
3007 FORMAT('O ETA FIELD (TEMPERATURE DEPENDANCE OF RQ*0)')
3008 FORMAT('O',///' ACCELERATION CRITERIA, W, WAS SPECIFIED AS ZERO.
      WAS THIS WOULD NOT ENABLE THE PROBLEM TO BE SOLVED,',/, ' THE VALUE
      HAS BEEN RESET TO 1.5')
3009 FORMAT('O FIRST ORDER ACCELERATION WILL BE USED FOR INNER LOOP ITERATION.',/, ' W = ',1PE10.3)
3012 FORMAT('!', 'PROGRAMME TERMINATING DUE TO UNEXPECTED END OF INPUT DATA (SUBROUTINE CASIN)')
3013 FORMAT('O')
3014 FORMAT('! UNIFORM TEMPERATURE ASSUMED.')
3015 FORMAT('O REQUESTED TO RUN PROGRAMME FOR ',I4,' OUTER LOOPS, EACH
      OF ',I4,' INNER LOOPS.')

```

C
END

C
SUBROUTINE TRVIAL (RD,IMAX,JMAX)

C
CHECK INPLT FOR TRIVIAL CASES.

C
COMMON /AREA/ AREA
COMMON /MCLWTS/ AM,BM
COMMON /NBF/ NBF

C
IF (IMAX*JMAX.GT.2000) GO TO 1000
IF (IMAX.LE.0.OR.JMAX.LE.0) GO TO 1001
DM=AM-AM
IF (DM.EQ.0) GO TO 1002
IF (AM.LE.0.OR.EM.LE.0) GO TO 1003
IF (AREA.LE.0) GO TO 1004
IF (RD.EQ.0) GO TO 1005
1007 IF (NBF.LE.0) GO TO 1006
WRITE(3,3007)
RETURN

C
1000 WRITE(3,3000)
STOP
1001 WRITE(3,3001)
STOP
1002 WRITE(3,3002)
STOP
1003 WRITE(3,3003)
STOP
1004 WRITE(3,3004)
STOP
1005 WRITE(3,3005)
RD=1.C
GO TO 1007
1006 WRITE(3,3006)
STOP

C
3000 FORMAT('!', 'MESH SIZE HAS BEEN SPECIFIED AS GREATER THAN 2000 O PR
PROBLEM IS TOO LARGE FOR THE PROGRAMME.',/, ' REDEFINE THE PROBLEM WI

```

      2TH LESS MESH SPACES.')
```

3001	FORMAT('1', 'MESH HAS BEEN SPECIFIED WITH IMAX OR JMAX AS ZERO OR	3930
	NEGATIVE. PROGRAMME TERMINATING.')	3940
3002	FORMAT('1', 'ISOTOPES A + B HAVE SAME MOLECULAR WEIGHT SO THERE IS	3950
	NO PROBLEM TO SOLVE. PROGRAMME TERMINATING.')	3960
3003	FORMAT('1', 'ONE ISOTOPE HAS ZERO MOLECULAR WEIGHT SO THERE IS NO	3970
	PROBLEM TO SOLVE. PROGRAMME TERMINATING.')	3980
3004	FORMAT('1', 'CHARACTERISTIC AREA SPECIFIED AS ZERO OR NEGATIVE. PRO	3990
	BLEM HAS NO PHYSICAL SIZE. PROGRAMME TERMINATING.')	4000
3005	FORMAT('1', 'RD SPECIFIED AS ZERO. VALUE OF RD=1.0 WILL BE SUBSTITU	4010
	TED.')	4020
3006	FORMAT('1', 'CONCENTRATION MUST BE DEFINED FOR AT LEAST ONE POINT. '	4030
	1,/, ' PROGRAMME TERMINATING.')	4040
3007	FORMAT('0 ', '///, ' DATA CHECK "TRVIAL" COMPLETED.')	4050
	END	4060
		4070
C	SUBROUTINE MESHIN(AMESH,MAXDIM)	4080
C		4090
C	SUBROUTINE TO READ IN MESH SPACINGS.	4100
C		4110
	DIMENSION AMESH(MAXDIM)	4120
	READ(1,2000) IN	4130
	IF(IN.EQ.) GC TO 1000	4140
	READ(1,2002)(AMESH(I),I=1,MAXDIM)	4150
	GC TO 1001	4160
1000	I=1	4170
	NN=0	4180
1003	READ(1,2001) A,N	4190
	NN=NN+N	4200
	DO 1002 J=1,NN	4210
1002	AMESH(J)=A	4220
	I=NN+1	4230
	IF(NN.LT.MAXDIM) GC TO 1003	4240
1001	DO 1004 I=1,MAXDIM	4250
	IF(AMESH(I).LE.0.0) GC TO 1005	4260
1004	WRITE(3,3000)AMESH(I)	4270
	RETURN	4280
3005	WRITE(3,3001) I,AMESH(I)	4290
	STOP	4300
2000	FORMAT(I3)	4310
2001	FORMAT(E6.0,I3)	4320
2002	FORMAT(1.2E6,C)	4330
3000	FORMAT(12(1X,'PF10.3))	4340
3001	FORMAT(' MESH INTERVAL SPECIFIED AS ZERO OR NEGATIVE. POINT IS=',	4350
	I3,' INTERVAL VALUE=',1PE10.3,/, ' PROGRAMME TERMINATING.')	4360
	END	4370
	SUBROUTINE FLOWIN (WR,WZ,IMAX,JMAX)	4380
C		4390
C	READ IN FLOW FIELD	4400
C		4410
	COMMON /LIMITS/ IMP1,IMP2,JMP1,JMP2	4420
	DIMENSION WR(IMP2,JMP2),WZ(IMP2,JMP2)	4430
C		4440
C	SET LOOP LIMITS	4450

C		4460
	IM=IMAX	4470
	IK=0	4480
	II=1	4490
1000	IF(IM.LE.10) GO TO 1001	4500
	IK=IK+10	4510
	GO TO 1002	4520
1001	IK=IM	4530
1002	DO 1003 J=1,JMAX	4540
	IKP1=IK+1	4550
	READ(1,2001)(WZ(I,J),I=II,IK)	4560
1003	READ(1,2000)(WR(I,J),I=II,IKP1)	4570
	READ(1,2001)(WZ(I,JMP1),I=II,IK)	4580
	IF(IM.LE.10) GO TO 1004	4590
	IM=IM-10	4600
	II=IK+1	4610
	GO TO 1000	4620
1004	CONTINUE	4630
	WRITE(3,3001)	4640
	II=1	4650
	IK=0	4660
	IM=IMAX	4670
1005	IF(IM.LE.6) GO TO 1006	4680
	IK=IK+6	4690
	GO TO 1007	4700
1006	IK=IM+IK	4710
1007	IKP1=IK+1	4720
	WRITE(3,3000)	4730
	DO 1008 J=1,JMAX	4740
	WRITE(3,3002)(WZ(I,J),I=II,IK)	4750
1008	WRITE(3,3003)((WR(I,J),I,J),I=II,IK),WR(IKP1,J)	4760
	WRITE(3,3002)(WZ(I,JMP1),I=II,IK)	4770
	IF(IM.LE.6) GO TO 1009	4780
	IM=IM-6	4790
	II=IK	4800
	GO TO 1005	4810
1009	CONTINUE	4820
	RETURN	4830
2000	FORMAT(12E6.0)	4840
2001	FORMAT(E9.0,10E6.0)	4850
3000	FORMAT('0',////)	4860
3001	FORMAT('1', 'FLCW FIELD')	4870
3002	FORMAT('0',6(10X,1PE10.3))	4880
3003	FORMAT('0',6(1PE10.3, '(,I3,',',',I3,')',1X),1PE10.3)	4890
	FNC	4900
	SUBROUTINE FLWCHK (MP,WZ,IMAX,JMAX)	4910
C		4920
C	CHECK WR(1,J)=C, IE: NO FLCW RADIALLY ACROSS CENTRE LINE.	4930
C	PRINT OUT ANY OFFENDERS.	4940
C		4950
	COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2	4960
	DIMENSION WR(IMP2,JMP2),WZ(IMP2,JMP2)	4970
	DO 1000 J=1,JMAX	4980
1000	IF(WR(1,J).NE.0.) WRITE(3,2000)J,WR(1,J)	4990

1002	FORMAT('0', 'NN=', I2, ' NM=', I2)	5550
1000	FORMAT(2I2)	5560
	IF(NN-2) GO TO 1103, 1104, 1102	5570
1104	CALL FREAD(P, IMAX, JMAX, NS)	5580
	WRITE(2, 1200)	5590
1200	FORMAT('12', 'NEW PRESSURE FIELD')	5600
	CALL FPRINT (P, IMAX, JMAX)	5610
	NN=-1	5620
	RETURN	5630
1102	CALL FREAD(T, IMAX, JMAX, NS)	5640
	WRITE(2, 1201)	5650
1201	FORMAT('1 NEW ETA FIELD')	5660
		5670
		5680
	CALL FPRINT (T, IMAX, JMAX)	5690
	NN=-1	5700
	RETURN	5710
1102	IF(NN.NF.-2) GO TO 1301	5720
	CALL FLWIN (WR, WZ, IMAX, JMAX)	5730
	CALL FLWCHK (WR, WZ, IMAX, JMAX)	5740
	NN=0	5750
	RETURN	5760
1101	CONTINUE	5770
	IF(NN) 1001, 1002, 1003	5780
1001	READ(1, MCLWT)	5790
	WRITE(3, MCLWT)	5800
	CALL TRVIAL (PC, IMAX, JMAX)	5810
	DO 1400 II=1, NM	5820
	READ(1, 1401) CH, I, J, VAL	5830
	WRITE(3, 1304) CH, I, J, VAL	5840
	IF(CH.EQ.PF) GO TO 1402	5850
	IF(CH.EQ.TT) GO TO 1403	5860
	WRITE(3, 1305)	5870
	GO TO 1400	5880
1402	P(I, J)=VAL	5890
	GO TO 1400	5900
1403	T(I, J)=VAL	5910
1400	CONTINUE	5920
1401	FORMAT(A1, 2(1X, I3), 2X, E13.6)	5930
	IF(NN.EQ.-2) GO TO 1002	5940
	GO TO 1004	5950
1002	DO 1300 II=1, NM	5960
	READ(1, 1301) CH, I, J, VAL	5970
	WRITE(3, 1304) CH, I, J, VAL	5980
	IF(CH.EQ.WRP) GO TO 1302	5990
	IF(CH.EQ.WZZ) GO TO 1303	6000
	IF(CH.EQ.REO) GO TO 1306	6010
	WRITE(3, 1305)	6020
	GO TO 1300	6030
1302	WR(I, J)=VAL	6040
	GO TO 1300	6050
1306	RD=VAL	6060
	GO TO 1300	6070
1303	WZ(I, J)=VAL	6080
1300	CONTINUE	6090
1301	FORMAT(A2, 2(1X, I3), 2X, E13.6)	6100
1304	FORMAT('0', A2, '(', I3, ' ', ' ', I3, ') = ', 1PE13.6)	6110
1305	FORMAT('+', 30X, 'ERRCR IN FORMAT.')	6120

CALL FLWCHK (WR,WZ,IMAX,JMAX)	613
IF(NN.EQ.-2) GO TO 1003	614
GO TO 1004	615
1007 ACC1=ACC	616
ND=NSPFD	617
A1=ALAMAX	618
A2=ALAMIN	619
READ(1,NEWACC)	620
WRITE(3,NEWACC)	621
IF(ND.NE.NSPFD.OR.A1.NE.ALAMAX.OR.A2.NE.ALAMIN) CALL EIGENV (ALPH	622
TA,BETA)	623
C	624
C IF NEW ACC GT OLD ACC, CASE WILL BE BYPASSED.	625
C	626
IF(ACC.LE.ACC1) GO TO 1004	627
WRITE(3,12C2) ACC	628
1202 FORMAT('D NEW ACCURACY IS NOT LESS THAN FOR PREVIOUS CASE,NO USEFU	629
1L RESULT WOULD BE PRODUCED.',/,,' PROGRAMME WILL BYPASS THIS CASE.'	630
2)	631
NN=5	632
RETURN	633
1004 NN=NN	634
IF(NN.EQ.-2) NN=-1	635
RETURN	636
END	637
C	638
C SUBROUTINE IDENTY (N,NS,IMAX,JMAX,IMP1,IMP2,JMP1,JMP2)	639
C	640
C SET NS=0 FOR ELEMENTS OUTSIDE SIMPLE PROBLEM BOUNDARIES AND NS=N	641
C FOR ALL DEFINED POINTS. HENCE, NS=0 FOR EXTERNAL POINTS,	642
C NS=1 FOR INTERNAL POINTS, NS=2 FOR EXTERNAL POINTS WITH DEFINED	643
C CONCENTRATION, F(I,J)	644
C	645
DIMENSION N(IMP1,JMP1),NS(IMP2,JMP2)	646
DO 2020 I=1,IMP2	647
NS(I,1)=0.C	648
2020 NS(I,JMP2)=0.0	649
DO 2021 J=1,JMP2	650
NS(I,J)=0.0	651
2021 NS(IMP2,J)=0.0	652
DO 2023 J=1,JMAX	653
DO 2022 I=1,IMAX	654
IF(NS(I+1,J+1).EQ.2) GO TO 2022	655
NS(I+1,J+1)=N(I,J)	656
2022 CONTINUE	657
2023 CONTINUE	658
C	659
C PRINT OUT VALUES OF NS(I,J)	660
C	661
WRITE(3,1117)	662
DO 2024 J=1,JMP2	663
2024 WRITE(3,1118)(NS(I,J),I=1,IMP2)	664
RETURN	665
1117 FORMAT('1', 'VALUES OF NS',/,/,5X, 'NS=0 -EXTERNAL',/,/,5X, 'NS=1 -INTER	666
1118 FORMAT('0',2X,22(2X,12))	667
END	668

	SUBROUTINE FCOEFF (AR,AZ,CR,DZ,DR,OZ,R,IMAX,JMAX)	7290
		7300
C		7310
C	FINITE ELEMENT COEFFICIENTS	7320
C		7330
	COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2	7340
	COMMON/AREA/ AREA	7350
	DIMENSION AR(IMAX,JMAX),AZ(JMAX),DR(IMP1),OZ(JMP1),	7360
	OR(IMAX),OZ(JMAX),R(IMP1)	7370
	PI=3.14159265	7380
	R(1)=0.0	7390
	R(2)=DR(1)	7400
	AZ(1)=PI*R(2)*CR(1)/AREA	7410
	OR(1)=1.0	7420
	OZ(1)=1.0	7430
	DO 2102 J=1,JMAX	7440
2102	AR(I,J)=0.0	7450
	DO 2100 I=2,IMAX	7460
	OR(I)=OR(I-1)/(CR(I)+DR(I-1))	7470
	R(I+1)=R(I)+OR(I)	7480
	AZ(1)=PI*(R(I+1)+R(I))*OR(I)/AREA	7490
	AR(I,1)=2.*PI*R(I)*OZ(1)/AREA	7500
	DO 2101 J=2,JMAX	7510
	AR(I,J)=2.*PI*R(I)*OZ(J)/AREA	7520
2101	OZ(J)=DZ(J)/(DZ(J)+DZ(J-1))	7530
2100	CONTINUE	7540
	RETURN	7550
	END	7560
	SUBROUTINE CDIFF (CR,CZ,AR,AZ,DR,DZ,T,NS,IMAX,JMAX,C3,C4)	7570
C		7580
C	CONCENTRATION DIFFUSION TERM	7590
C		7600
	COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2	7610
	DIMENSION AR(IMAX,JMAX),AZ(JMAX),DR(IMP1),OZ(JMP1),	7620
	T(IMAX,JMAX),NS(IMP2 ,JMP2),C3(JMAX),C4(JMAX),CR(IMAX,JMAX),	7630
	OZ(IMAX,JMAX)	7640
	DO 1000 I=1,IMAX	7650
	IS=I+1	7660
	DO 1000 J=1,JMAX	7670
	JS=J+1	7680
	IF(NS(IS,JS).EQ.0) GO TO 1000	7690
	IF(JS.NE.2) GO TO 1001	7700
	C1=OZ(1)/T(I,1)	7710
1001	IF(IS.NE.2) GO TO 1002	7720
	C3(J)=DR(1)/T(1,J)	7730
1002	C2=OZ(J)/T(I,J)	7740
	C4(J)=DR(I)/T(I,J)	7750
	IF(NS(IS,J).EQ.0) GO TO 1003	7760
	CZ(I,J)=2.*AZ(I)/(C1+C2)	7770
	C1=C2	7780
1003	IF(NS(I,JS).EQ.0) GO TO 1000	7790
	CR(I,J)=2.*AR(I,J)/(C3(J)+C4(J))	7800
	C3(J)=C4(J)	7810
1000	CONTINUE	7820
	RETURN	7830
	END	7840

	SUBROUTINE PDIFF (F,AF,AZ,S,F,T,PD,DR,DZ,NS,IMAX,JMAX, U3,U4,J2,LZ)	7850
		7860
		7870
	PRESSURE DIFFUSION TERM	7880
		7890
	COMMON /MCLN/TS/ AM,BM	7900
	COMMON /LIMITS/ IVP1,IMP2,JMP1,JMP2	7910
	DIMENSION F(IMAX,JMAX),AP(IMAX,JMAX),AZ(JMAX),S(IMAX,JMAX), P(IMAX,JMAX),T(IMAX,JMAX),DR(IMP1),DZ(JMP1),NS(IMP2,JMP2), U3(IMP2),U4(IMP2),UR(IMP2,JMP2),LZ(IMP2,JMP2)	7920
	DM=5M-AM	7930
	DUMY=1./(2.*DM*PD)	7940
		7950
		7960
		7970
	START OF OUTER ITERATION LOOP	7980
		7990
	DO 1006 I=1,IMP1	8000
	IS=I+1	8010
	DO 1006 J=1,JMP1	8020
	JS=J+1	8030
	IF(NS(IS,JS).EQ.0) GO TO 1008	8040
	PDUM=DUMY/(T(I,J)*F(I,J)+(1.-F(I,J))*(F(I,J)/AM+(1.-F(I,J))/BM))	8050
	IF(JS.NE.2) GO TO 1000	8060
	U1=DZ(I)*PDUM	8070
1000	IF(IS.NE.2) GO TO 1001	8080
	U3(J)=DR(I)*PDUM	8090
1001	CONTINUE	8100
	U2=DZ(J)*PDUM	8110
	U4(J)=DR(I)*PDUM	8120
	IF(NS(IS,J).EQ.0) GO TO 1002	8130
	PZ=P(I,J-1)/P(I,J)	8140
	IF(PZ.EQ.1) GO TO 1002	8150
	LZ(I,J)=AZ(I)*ALOG(PZ)/(U1+U2)	8160
	GO TO 1003	8170
1002	UZ(I,J)=0.0	8180
1003	U1=U2	8190
	IF(NS(I,JS).EQ.0) GO TO 1004	8200
	PR=P(I-1,J)/P(I,J)	8210
	IF(PR.EQ.1) GO TO 1004	8220
	UR(I,J)=AP(I,J)*ALOG(PR)/(U3(J)+U4(J))	8230
	GO TO 1005	8240
1004	UR(I,J)=0.0	8250
1005	U3(J)=U4(J)	8260
1006	CONTINUE	8270
	DO 1007 I=1,IMAX	8280
	IS=I+1	8290
	DO 1007 J=1,JMAX	8300
	JS=J+1	8310
	IF(NS(IS,JS).EQ.0) GO TO 1007	8320
	S(I,J)=UR(I,J)+UZ(I,J)-UR(IS,J)-UZ(I,JS)	8330
1007	CONTINUE	8340
	RETURN	8350
1008	UZ(I,J)=0.0	8360
	UR(I,J)=0.0	8370
	GO TO 1006	8380
	END	8390

```

SUBROUTINE ILPREP (WR,WZ,CZ,QZ,CR,CZ,HL,HR,HU,HC,SUM,NS,IMAX,JMAX)  8400
C  PREPARATION OF SUM,AND HD,HL,FL,FR FOR INNER ITERATION  8410
C  COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2  8420
C  DIMENSION WR(IMP2,JMP2),WZ(IMP2,JMP2),  8430
C  QR(IMAX),QZ(JMAX),CR(IMAX,JMAX),CZ(IMAX,JMAX),HL(IMAX,JMAX),HR(IMA  8440
C  X,JMAX),HU(IMAX,JMAX),FC(IMAX,JMAX),SUM(IMAX,JMAX),NS(IMP2,JMP2)  8450
C  K=1  8460
C  DO 1012 I=1,IMAX  8470
C  IS=I+1  8480
C  DO 1012 J=1,JMAX  8490
C  JS=J+1  8500
C  IF(NS(IS,JS).NE.1) GO TO 1012  8510
C  IF(NS(I,JS).EQ.0) GO TO 1000  8520
C  HD(I,J)=CR(I,J)+ WR(I,J)*QR(I)  8530
C  GO TO 1001  8540
1000 HD(I,J)=0.0  8550
C  IF(WR(I,J).GT.0.0) HD(I,J)=WR(I,J)  8560
1001 IF(NS(IS,J).EQ.0) GO TO 1002  8570
C  HL(I,J)=CZ(I,J)+ WZ(I,J)*QZ(J)  8580
C  GO TO 1003  8590
1002 FL(I,J)=0.0  8600
C  IF(WZ(I,J).GT.0.0) HL(I,J)=WZ(I,J)  8610
1003 IF(NS(IS+1,JS).EQ.0) GO TO 1004  8620
C  HU(I,J)=CR(IS,J) *WR(IS,.)*(1.-QR(IS))  8630
C  GO TO 1005  8640
1004 HU(I,J)=0.0  8650
C  IF(WR(IS,J).LT.0.0) HU(I,J)=-WR(IS,J)  8660
1005 IF(NS(IS,JS+1).EQ.0) GO TO 1006  8670
C  HR(I,J)=CZ(I,JS) *WZ(I,JS)*(1.-CZ(JS))  8680
C  GO TO 1007  8690
1006 HR(I,J)=0.0  8700
C  IF(WZ(I,JS).LT.0.0) HR(I,J)=-WZ(I,JS)  8710
1007 SUM(I,J)=HR(I,J)+HU(I,J)+FL(I,J)+HD(I,J)  8720
C  IF(HL(I,J).LT.0.0) GO TO 1013  8730
1008 IF(HR(I,J).LT.0.0) GO TO 1014  8740
1009 IF(HU(I,J).LT.0.0) GO TO 1015  8750
1010 IF(HD(I,J).LT.0.0) GO TO 1016  8760
1011 IF(SUM(I,J).EQ.0) WRITE(3,3000) I,J  8770
1012 CONTINUE  8780
C  IF(K.EQ.1) WRITE(3,3001)  8790
C  RETURN  8800
1013 IF(K.EQ.1) WRITE(3,3002)  8810
C  CALL UNSTBL (1,J,CZ(I,J), WZ(I,J),QZ(J))  8820
C  K=K+1  8830
C  GO TO 1008  8840
1014 IF(K.EQ.1) WRITE(3,3002)  8850
C  CALL UNSTBL (2,JS,CZ(I,JS) ,WZ(I,JS),QZ(JS)-1.)  8860
C  K=K+1  8870
C  GO TO 1009  8880
1015 IF(K.EQ.1) WRITE(3,3002)  8890
C  CALL UNSTBL (3,IS,CR(IS,J) ,WR(IS,J),QR(IS)-1.)  8900
C  K=K+1  8910
C  GO TO 1010  8920
1016 IF(K.EQ.1) WRITE(3,3002)  8930
C  CALL UNSTBL (4,I,CR(I,J), WR(I,J),QR(I))  8940
C  K=K+1  8950
C  GO TO 1011  8960
2000 FFORMAT('0','SUM(',I3,',',I2,')=0.0')  8970

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3001	FORMAT('O ALL FF COEFFICIENTS ACCEPTED AS GE ZERO FOR STABILITY')	9000
3002	FORMAT('I WARNING--THIS PROBLEM MAY BE UNSTABLE AND NOT CONVERGE.'	9010
	1,/, 'O STABILITY AND CONVERGENCE MAY BE ACHIEVED BY USING A FINER M	9020
	2ESH. ',/, 'O SUGGESTED ACTIONS : ',//)	9030
	END	9040
	SUBROUTINE INLCOP (F,FM1,FP1,S,HL,HR,HU,HD,SUM,NS,IMAX,JMAX)	9050
C		9060
C	INNER ITERATION FOR CONCENTRATIONS	9070
C		9080
	COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2	9090
	COMMON /ACC/ ACC,EMAX1,ALPHA,BETA,NJ,W,NSPEED,NINNER,NO OUTER	9100
	DIMENSION F(IMAX,JMAX),FM1(IMAX,JMAX),FP1(IMAX,JMAX),	9110
	IS(IMAX,JMAX),FL(IMAX,JMAX),HR(IMAX,JMAX),HU(IMAX,JMAX),HD(IMAX,JMA	9120
	EX),SUM(IMAX,JMAX),NS(IMP2,JMP2)	9130
	K=0	9140
	EMAX2=0.0	9150
	AA=100.0	9160
	SMLACC=0.0	9170
	WRITE(3,3002)	9180
	CALL FPRINT(F,IMAX,JMAX)	9190
	JCT=0	9200
1000	EMAX1=0.0	9210
	JCT=JCT+1	9220
	DO 1002 I=1, IMAX	9230
	IS=I+1	9240
	DO 1002 J=1, JMAX	9250
	JS=J+1	9260
	IF(NS(IS,JS).NE.1) GO TO 1002	9270
	FN=(S(I,J)+HD(I,J)*F(I-1,J)+HL(I,J)*F(I,J-1)+HU(I,J)*F(I+1,J)+HR(I	9280
	1,J)*F(I,J+1))/SUM(I,J)	9290
	ERR=ABS(FN-F(I,J))	9300
C	CHECK THAT STEPS IN F ARE NOT TOO GREAT AS TO INVALIDATE PRESENT	9310
C	COEFFICIENTS, IF THEY ARE, SET K TO RETURN TO OUTER LOOP AFTER 2ITN	9320
	IF(ERR.GT.F(I,J)/2.0) K=K+6	9330
	IF(ERR.GT.EMAX1) EMAX1=ERR	9340
	IF(NSPEED.EQ.1) GO TO 1001	9350
	F(I,J)=W*FN+(1.-W)*F(I,J)	9360
	GO TO 1002	9370
1001	FP1(I,J)=F(I,J)*(1.+ALPHA-BETA)-FM1(I,J)*ALPHA+FN*BETA	9380
1002	CONTINUE	9390
	IF(NSPEED.EQ.1) CALL RESET (F,FM1,FP1,NS,IMAX,JMAX)	9400
	IF(JCT/AA.LE.1.0) GO TO 1003	9410
	AA=AA+100.0	9420
	WRITE(3,3002)	9430
	CALL FPRINT(F,IMAX,JMAX)	9440
1003	CONTINUE	9450
C		9460
C	CHECK CONVERGENCE OF INNER ITERATION	9470
C		9480
	IF(EMAX2.LT.SMLACC) SMLACC=EMAX2	9490
	IF(EMAX1.GE.SMLACC)K=K+1	9500
	IF(NINNER.GT.JCT.CR.NINNER.LT.1.CR.NO OUTER.LT.1) GO TO 1008	9510
	WRITE(3,3005)	9520
	RETURN	9530
1008	IF(K-500) 1006,1004,1005	9540
1004	WRITE(3,3004) ACC,JCT	9550

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IF (JCT.CE.50) RETURN 956
IF (NSPFD.EQ.0.AND.JCT.LT.500) GO TO 1000 957
NJ= 958
RETURN 959
1005 IF (NSPFD.EQ.0.AND.JCT.LT.500) GO TO 1000 960
WRITE(3,3000) 961
RETURN 962
1006 FMAX2=FMAX1 963
C 964
C CHOOSE CONVERGENCE TOLERANCE FOR INNER LOOP TO BE 1/10 OF MAX 965
C CHANGE ON FIRST ITERATION OR ACC WHICHEVER IS LEAST. 966
C 967
IF (JCT.NE.1) GO TO 1007 968
TOL=FMAX2/10. 969
IF (TOL.LT.ACC) TOL=ACC 970
SMACC=FMAX2 971
1007 IF (FMAX1.GT.TOL) GO TO 1000 972
IF (NSPFD.EQ.0.AND.JCT.LT.500) GO TO 1000 973
WRITE(3,3001) TOL 974
WRITE(3,3003) JCT 975
RETURN 976
3000 FORMAT(' INNER ITERATION HAS CHANGED CONC BY 50%, RETURNING TO OUT 977
ER LOOP TO RECALCULATE COEFFICIENTS. ') 978
3001 FORMAT(' CONVERGENCE TOLERANCE FOR THIS ITERATION = ',1PE10.3) 979
3002 FORMAT(' ') 980
3003 FORMAT(' INNER LOOP CONVERGED IN ',I4,' ITERATIONS. ') 981
3004 FORMAT(' INNER ITERATION NOT CONVERGING TO REQUIRED ACCURACY,(= ', 982
1PE10.3,' ). AFTER ',I3,' ITERATIONS, RETURNING TO OUTER LOOP. ') 983
3005 FORMAT(' REQUESTED NUMBER OF INNER LOOPS COMPLETED. ') 984
END 985

SUBROUTINE PREAD (X,NS,IMAX,JMAX) 986
C 987
C SUBROUTINE TO READ IN VARIOUS FIELDS. 988
C 989
DIMENSION X(12,120) 990
DO 1000 J=1,JMAX 991
READ(1,1001)(X(I,J),I=1,IMAX) 992
DO 1002 I=1,IMAX 993
IF (X(I,J).LE.0) GO TO 2000 994
1002 CONTINUE 995
1000 CONTINUE 996
RETURN 997
2000 IF (NS(I+1,J+1).EQ.0) GO TO 1002 998
WRITE(3,1003) I,J,X(I,J) 999
STOP 1000
1001 FORMAT(12F6.0) 1001
1003 FORMAT(' ', 'ELEMENT OF PRESSURE OR TEMPERATURE FIELD SPECIFIED AS 1002
ZERO OR NEGATIVE. THIS HAS NO PHYSICAL MEANING. ',/, ' POINT IS, ( ', 1003
I3,', ',I3,' ). ELEMENT VALUE WAS =',1PE10.3,/, ' PROGRAMME TERMINATI 1004
NG ') 1005
END 1006

```

	SUBROUTINE FPRINT(X,IMAX,JMAX)	10070
C		10080
C	SUBROUTINE TO PRINT OUT VARIOUS FIELDS	10090
C		10100
	DIMENSION X(IMAX,JMAX)	10110
	II=1	10120
	IK=0	10130
	IM=IMAX	10140
2220	IF(IM.LE.8) GO TO 2221	10150
	IK=IK+3	10160
	GO TO 2222	10170
2221	IK=IM+IK	10180
2222	DO 2223 J=1,JMAX	10190
2223	WRITE(3,1122)(X(I,J),I=II,IK)	10200
	IF(IM.LE.8) GO TO 2224	10210
	IM=IM-9	10220
	II=IK+1	10230
	WRITE(3,1121)	10240
	GO TO 2220	10250
2224	CONTINUE	10260
1121	FORMAT('0',//)	10270
1122	FORMAT('0',8(4X,1PE12.5))	10280
	RETURN	10290
	END	10300
	SUBROUTINE MXCNCH (F,FF,IMAX,JMAX,CONV2)	10310
C		10320
C	DETERMINE MAX CONC CHANGE IN LAST INNER LOOP AS CONV2	10330
C	UPDATE FF ARRAY TO PRESENT CCNCS.	10340
C		10350
	DIMENSION F(IMAX,JMAX),FF(IMAX,JMAX)	10360
	COMMON /CCNVRG/ CCNVI,KK	10370
C		10380
	CCNV2=0.0	10390
	DO 1000 I=1,IMAX	10400
	DO 1000 J=1,JMAX	10410
	C=ABS(F(I,J)-FF(I,J))	10420
	IF(C.LT.CCNV2) GO TO 1000	10430
	CCNV2=C	10440
	FF(I,J)=F(I,J)	10450
1000	CONTINUE	10460
	RETURN	10470
	END	10480
	SUBROUTINE CONDEF (F,FM1,FF1,N,IMAX,JMAX)	10490
C		10500
	DIMENSION F(IMAX,JMAX),FM1(IMAX,JMAX),FP1(IMAX,JMAX),N(IMAX,JMAX)	10510
	COMMON /NBF/ NFF	10520
	COMMON /TIGHT/ ACC1	10530
C		10540
C	READ IN PROBLEM BOUNDARIES N(I,J)	10550
C		10560
	WRITE(3,3004)	10570
	WRITE(3,3001)	10580
	READ(2,2000)((N(I,J),I=1,IMAX),J=1,JMAX)	10590
	WRITE(3,3002)((N(I,J),I=1,IMAX),J=1,JMAX)	10600
C		10610

```

C READ IN GIVEN CONCENTRATIONS F(I,J), CHECK THAT POSITION IS OUTSIDE 10620
C PROBLEM BOUNDARY 10630
C FORM ACC1 AS A TIGHT ACCURACY CRITERIA BASED ON THE DEFINED 10640
C CONCENTRATION AT LAST SPECIFIED POINT, NBF. 10650
C 10660
C DO 1000 II=1,NBF
C READ(1,2001) I,J,F(I,J) 10670
C ACC1=F(I,J)/1.0E+08 10680
C IF(N(I,J).EQ.1) WRITE(3,3000) I,J 10690
C IF(F(I,J).EQ.0.0.OR.F(I,J).EQ.1.0) GO TO 1001 10700
C 10710
1000 CONTINUE 10720
C RETURN 10730
1001 WRITE(3,3003) 10740
C STOP 10750
2000 FORMAT(35I2) 10760
2001 FORMAT(2I2,810.0) 10770
3000 FORMAT('1','ERROR IN INPUT',/, 'CONCENTRATION HAS BEEN DEFINED FOR
1 A POINT INSIDE THE SYSTEM BOUNDARY',/, 'POINT IS, I=',I3,2X, 'J=',
2 I2) 10780
3001 FORMAT('0 BOUNDARY SPECIFICATION') 10810
3002 FORMAT('0',33(2X,I2)) 10820
3003 FORMAT('1','CONCENTRATION FOR ARCV POINT HAS BEEN SPECIFIED AS 1.
10 OR 0.0 THESE VALUES ARE IMPOSSIBLE FOR A FINITE PROBLEM.',/,
2 'PROGRAMME TERMINATING.')
```

10830
10840
10850
3004 FORMAT('0') 10860
10870
10880

```

C
C END 10880

SUBROUTINE ACCTST (ACC) 10890
COMMON /TIGHT/ ACC1 10900
C 10910
C CHECK THAT INPUT ACC FIGURE IS SUFFICIENTLY SMALL TO GIVE A 10920
C MEANINGFUL ANSWER. IF IT IS NOT, PRINT RECOMMENDED VALUE. 10930
C 10940
C IF(ACC.LE.0.0) ACC=ACC1 10950
C IF(ACC.LT.ACC1) RETURN 10960
C WRITE(3,3001) 10970
C WRITE(3,3000) ACC1 10980
C RETURN 10990
3000 FORMAT('0 REQUESTED ACCURACY MAY NOT BE SUFFICIENTLY SMALL TO GIVE
1 A MEANINGFUL ANSWER.',/, 'RECOMMENDED VALUE FOR THIS CASE IS ACC=
2 ',1PE10.3) 11000
3001 FORMAT('0') 11030
C END 11040

SUBROUTINE UNSTBL (I,J,C, W,Q) 11050
GO TO (1000,1001,1002,1003),I 11060
1000 CONTINUE 11070
1001 WRITE(3,3000) J 11080
C GO TO 1004 11090
1002 CONTINUE 11100
1003 WRITE(3,3001) J 11110
1004 F=(W*Q /C) 11120
C WRITE(3,3003) F 11130
C RETURN 11140
3000 FORMAT('0 MAKE AXIAL MESH FINER AROUND J = ',I3, ' BY FACTOR OF ') 11150
3001 FORMAT('0 MAKE RADIAL MESH FINER AROUND I = ',I3, ' BY FACTOR OF ') 11160
3003 FORMAT('+',58X,1PE12.5) 11170
C END 11180
```

	SUBROUTINE RESET (F,FM1,FP1,NS,IMAX,JMAX)	11190
C		11200
C	SUBROUTINE TO UPDATE CCNC. VALLES AFTER EACH ITERATION LOOP	11210
C		11220
	COMMON/LIMITS/IMP1,IMP2,JMP1,JMP2	11230
	DIMENSION F(IMAX,JMAX),FM1(IMAX,JMAX),FP1(IMAX,JMAX),	11240
	1 NS(IMP2,JMP2)	11250
	DO 1000 I=1,IMAX	11260
	DO 1000 J=1,JMAX	11270
	IF(NS(I+1,J+1).EQ.2) GO TO 1000	11280
	FM1(I,J)=F(I,J)	11290
	F(I,J)=FP1(I,J)	11300
1000	CONTINUE	11310
	RETURN	11320
	END	11330
	SUBROUTINE FPUNCH(X,IMAX,JMAX)	11340
	DIMENSION X(IMAX,JMAX)	11350
	DO 1000 J=1,JMAX	11360
1000	WRITE(2,4000)(X(I,J),I=1,IMAX)	11370
	RETURN	11380
4000	FORMAT(6(1PE12.5))	11390
	END	11400
	SUBROUTINE RESTRT(X,IMAX,JMAX)	11410
	DIMENSION X(IMAX,JMAX)	11420
	DO 1000 J=1,JMAX	11430
1000	READ(1,2000)(X(I,J),I=1,IMAX)	11440
	RETURN	11450
2000	FORMAT(6(E12.5))	11460
	END	11470

